



شركة طاقة الشمال





اول نموذج متميز لتوليد الطاقة الكهربائية عبر معالجة النفايات عن طريق نظام التفكك الحراري

Waste - To -Energy

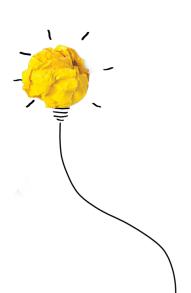




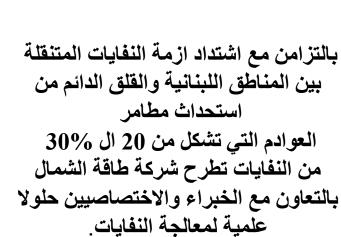


التصميم

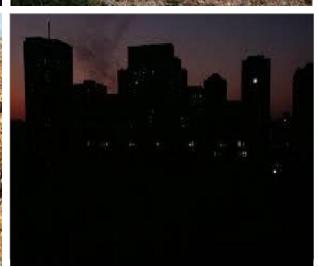
- 1- المقدمة
- 2- من نحن
- 3- لماذا نظام تفاعل حراري
- 4- لمحة عامة عن المشروع
 - 5- معايير سلامة البيئة
 - 6- طرق العمل
 - 7- الجدوى الاقتصادية
 - 8- القيمة المضافة



المقدمة

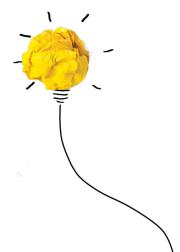












تاريخ الشركة

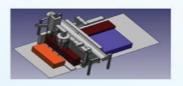
2005-2013

دراسات هندسية لصناعة محطة طاقة تجاربية محلية



2014

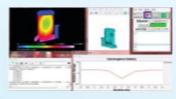
صناعة أول محطة تجاربية ولدت الكهرباء في رأسنحاش





2015

دراسات هندسية لزيادة القدرة الإنتاجية للمحطة وتفعيلها في طرابلس وبعض المدن الأخرى



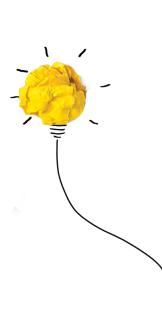


2016



المقدمة

2005



















Universities Public Research organizations

Survey research on industry-academia-government collaboration

Businesses Start-ups

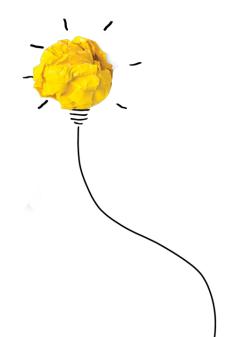
Survey research on the current status and issues of academic start-ups



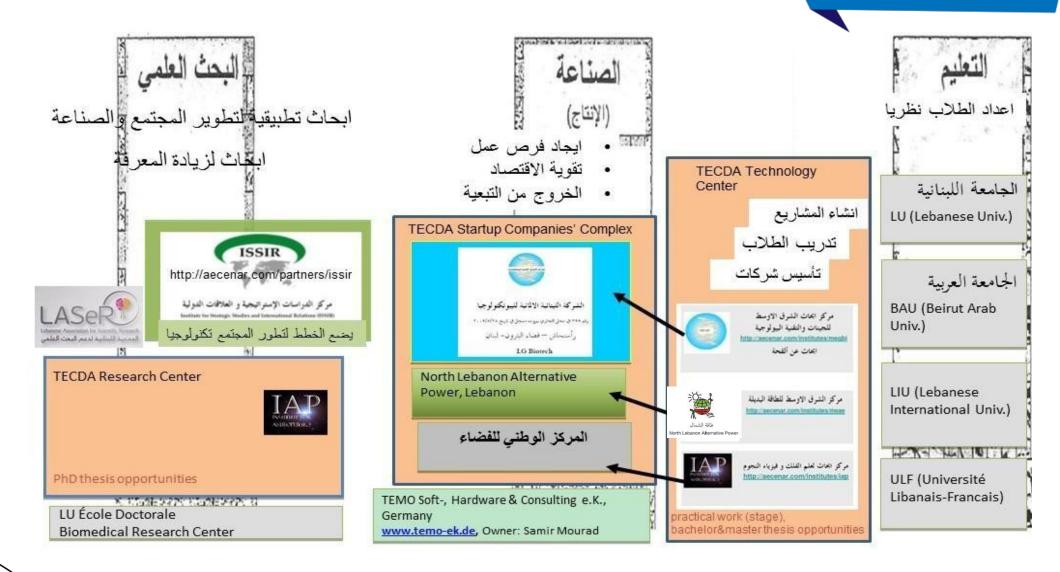
Government Local public entities

Survey research on regional innovation activities

- Research on regional innovation systems
- Case study on regional clusters (e.g.food industrial cluster)



من نحن

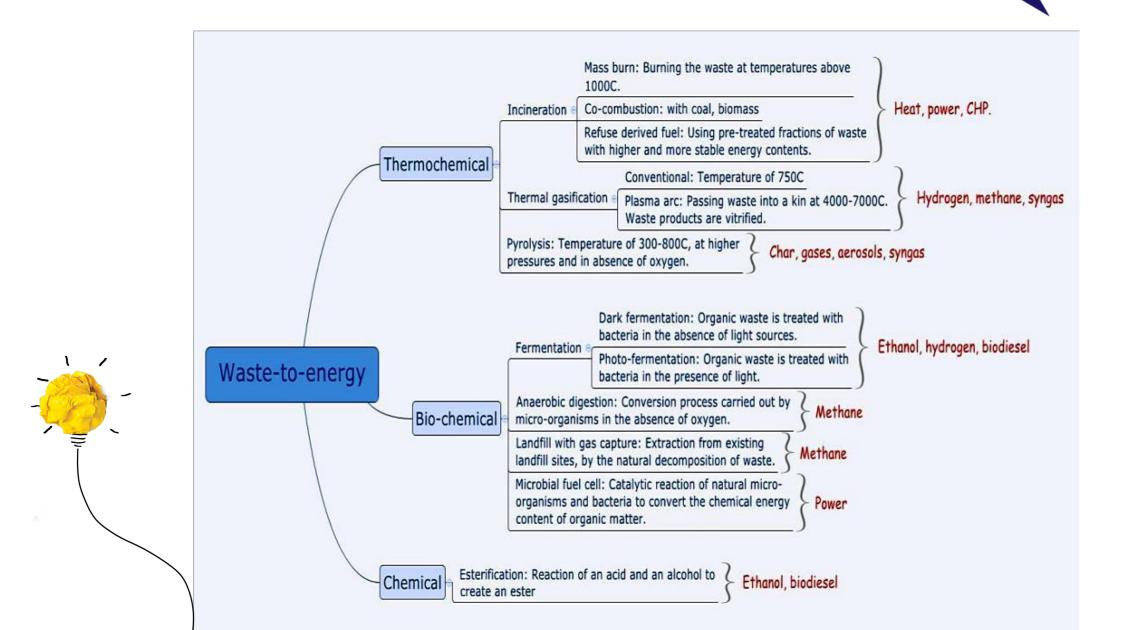


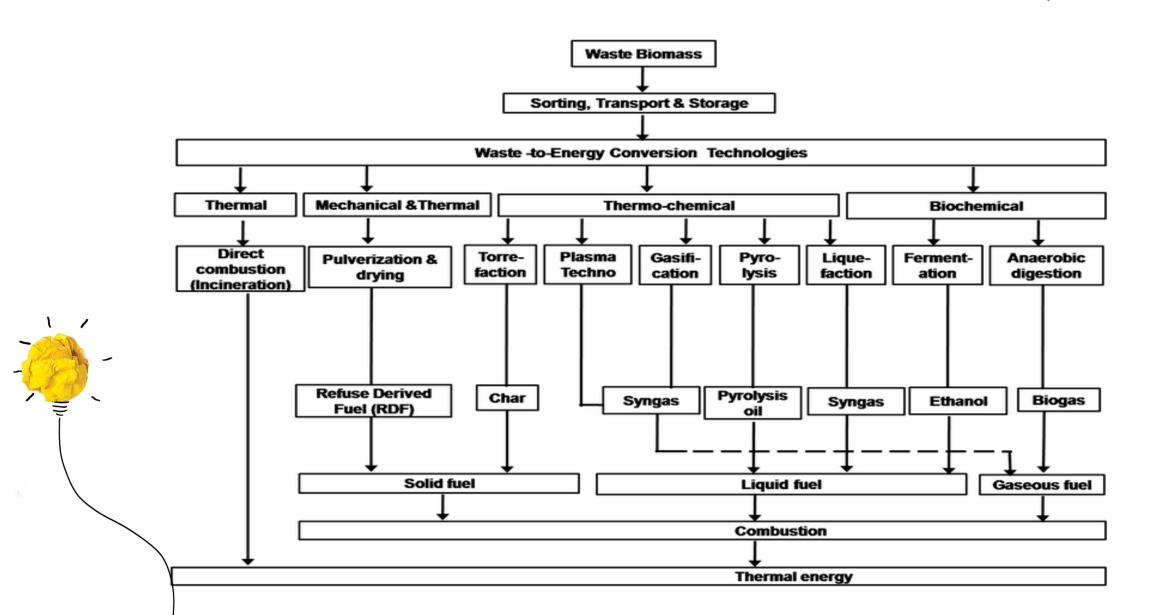






لماذا نظام التفكك الحراري

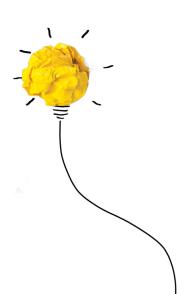


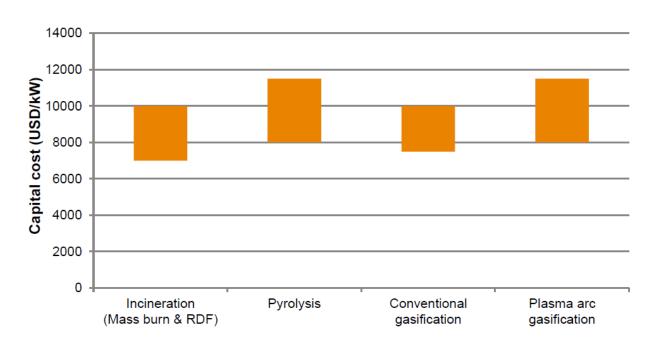


CAPITAL COSTS FOR THERMAL WTE POWER GENERATION TECHNOLOGIES IN THE UNITED STATES (15 MW OUTPUT)

The capital investments for the construction and implementation of these technologies, and the costs needed to operate them for the entire lifetime of a chosen project can influence decisions.

As of today, incineration of MSW still presents the most desirabandle economic conditions on the market, is therefore the preferred option in most markets.



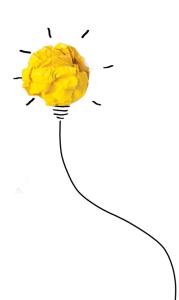


Source: Stringfellow (2014)

BIOMASS AND WASTE POLICY TARGETS IN SELECTED COUNTRIES

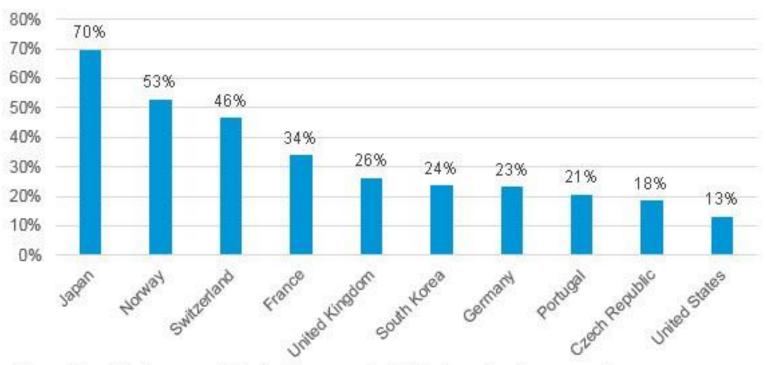
Country	Biomass and waste targets		
China	30 GW by 2020		
Germany	14% of heating by 2020		
Indonesia	810 MW by 2025		
Norway	14 TWh annual production by 2020		
Philippines	267 MW by 2030		
United States	Contained in state-level Renewable Portfolio Standards		





لماذا نظام التفكك الحراري

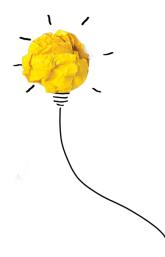
Percent of total municipal sold waste that is burned with energy recovery in selected countries



Note: Data for Japan and South Korea are for 2013. Data for other countries are for 2014.

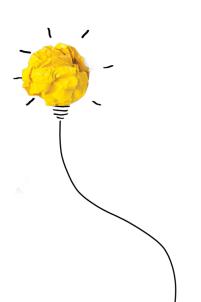
Source: U.S. Environmental Protection Agency for the United States, Organization for Economic Cooperation and Development for other countries

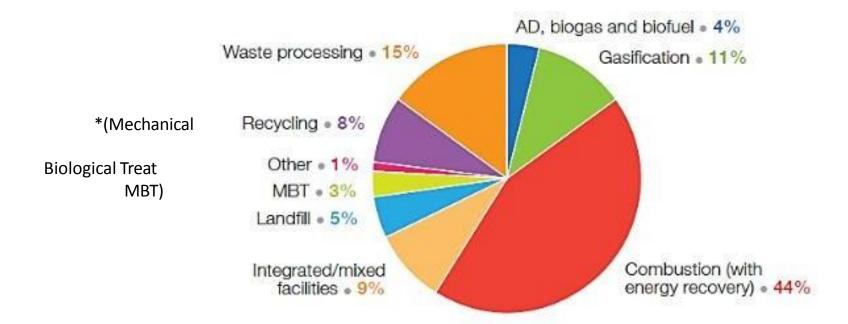




Utility Scale Plants existing according to the technology used.

(Data from 93 countries in 20132014 (total of 2723 facilities)).





لماذا نظام التفكك الحراري







Incinerator in world



The largest scale plant with the capacity to handle 4,320t/day was built in Singapore in only 38months Source: Mitsubishi Heavy Industries, Environmental & Chemical Engineering Co., Ltd.



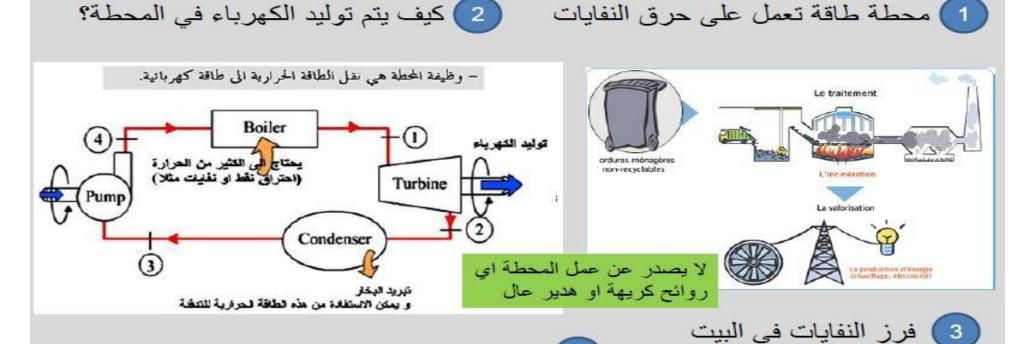
In Thailand, an industrial waste incinerator has been operating from 2006. Its treatment capacity is 100t/day. Source: JFE Engineering Corporation





لمحة عامة عن المشروع

ما لا يحرق في المحطة:



4 تنقية الدخان الناتج عن حرق النفايات

0

0

with 145 °C to

بعد تنقية

بيقي ما هو

مضر بالبيئة

الدخان المنبعث لا

سام او

thus gas from:

chamber (100°C)

لمحة عامة عن المشروع



Fraction	Net Calorific Value (MJ/kg)		
Paper	16		
Organic material	4		
Plastics	35		
Glass	0		
Metals	0		
Textiles	19		
Other materials	11		

Source: ISWA (2013)

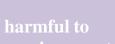


Residues of incineration of 1 ton of waste 700 kg of gas, 300 kg of solid residues including 30 kg of fly ash.

Division of emissions(depending on their size and the degree of severity:)



Nonharmful to the environment



Challenges



Nitrogen (N₂), Oxygen (O₂), and water vapor (H₂O)

Acid gases: nitrogen dioxide (NO₂), nitrogen oxide (NO), Sulfur dioxide (SO₂), carbon dioxide (CO₂),HCl, Dust

Furans, dioxins, heavy metals (Hg from batteries, cadmium, plumb, zinc)





1.Techniques for the reduction of nitrogen oxide

تقنيات للحد من اوكسيد النيتروجين

Thermal NOx: When burning a portion of the nitrogen in the air is oxidized to nitrogen oxides. This reaction occurs only significantly at temperatures above 1300 °C. The reaction rate depends exponentially on the temperature and is directly proportional to the oxygen content Fuel NOx: when burning a portion of the nitrogen contained in the fuel is oxidized to nitrogen oxides.



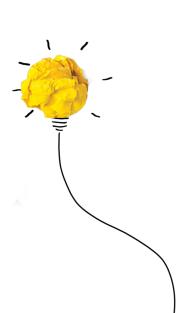
PROCESS OF REDUCING NONSELECTIVE CATALYTIC (SNCR):

the reducing agent (typically ammonia or urea) is injected into the furnace and reacts with nitrogen oxides. The reactions occur at temperatures between 850 and 1000 ° C, with higher reaction rates and lower in this range. To be effective, the catalyst generally requires a temperature between 180 and 450 ° C. The majority of systems uses waste incinerators currently operating at temperatures of the order of 230300 ° C.



Selective Catalytic Reduction (SCR) is a catalytic process during which ammonia mixed with air (the reduction agent) is added to the exhaust gas and passes through a catalyst, usually a sieve (e.g. Platinum, rhodium, TiO₂, zeolites). When passing through the catalyst, ammonia reacts with NOx to give nitrogen and water vapor.

تنقية دخان مصنع التفكك الحراري



ع ج النبو كمسين والفيوران 2.Treatment of dioxin and furans and mercury Hg & ∞2.

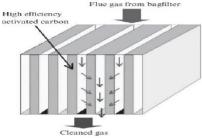
By activated carbon(can be also called "lignite Coke for odorous compounds.)
Activated carbon is in the form of a fine black talc. Its elementary particles are made porous by a suitable heat treatment so as to create therein pores having dimensions of affinity with the molecules to be filtered. So there are formulations of active carbon adapted to different molecules that one wishes to retain.

The Environmental Protection Agency(EPA) showed that dioxins broke down easily when exposed to temperatures in excess of 1,200 °C.

To obtain a minimum feeding rate (F(min)) of activated carbon (AC), It was found that dioxin removal efficiency(eta) increased with an increase in AC feeding concentration. This had an almost linear function to F/Q when F/Q was less than 65 g/Nm(3), where F was the AC feeding rate (mg/min), and Q was the volumetric flow rate of flue gas (Nm(³)/min). However, it did not seem to be affected by F/Q, when F/Q was larger than 150 mg/Nm(³). On the basis of the experimental data obtained in this study, the removal efficiency of dioxins by the application of AC could be correlated as eta (%)=100/[1.0+(40.2/(F/Q)(3))]. It is valid in appropriate conditions (F/Q=10300 mg/Nm(³)) suggested by the study with a statistical error of +/18%.

Intelligent Gravimetric
Analyzer (IGA)
The system is an ultrahigh
vacuum (UHV) system and
allows measurement of
isotherms and accurate
determination of the adsorption
and desorption kinetic profiles
for each pressure step.
The system consists of a
fully computer controlled
microbalance, pressure
admit system and
temperature regulation

Measurement: The



Cartridge packed with activated carbon

Dioxins concentrations at activated carbon adsorber Dioxins concentrations Removal-(ng-TEQ/m³-norm.) efficiency (%) Inlet Outlet Electric furnace for steel 5.5 0.009399.83 Ash melting furnace 1.8 0.00080 99.96 Waste furnace 1.1 0.000 16 99.99

Ref:Minimum feeding rate of activated carbon to control dioxin emissions from a largescale municipal solid waste incinerator, Article in Journal of Hazardous Materials 161(23):143643 · June 2008 with 289 Reads DOI: 10.1016/j.jhazmat.2008.04.128 · Source: PubMed

system

تنقية دخان مصنع التفكك الحراري

3.Acid gas treatment technologies(HF,HCl and SO₂)

تقنيات معالجة الغاز الحمضى



Depending on the concentrations, temperature, size of the flow to be treated and of further parameters, can be used different technologies for the treatment of acid gas emissions. Being a quick summary we can mention:

Bag filters with reagent injection(calcium hydroxide (Ca(OH)₂) or sodium bicarbonate))

The filters in flat bags are successfully used for the chemical absorption of acid gases such as HF, HCl and SO₂ in addition to the adsorption of other pollutant compounds.

Generally it is used, among others, calcium hydroxide and sodium bicarbonate (Ca(OH)₂) of typical commercial quality, which is injected in the gas stream before entering the filter. To achieve proper compliance with the emission limits required, the additive should be added in amounts overstoichiometric (from 1.5 to 3 times). at least 130200 ° C

• Treatment by Ca(OH)₂:

 $Ca(OH)_2 + 2HCl \leftrightharpoons CaCl_2 + 2H_2O$

 $Ca(OH)_2 + 2HF \Leftrightarrow CaF_2 + 2H_2O$

 $Ca(OH)_2 + SO_2 \leftrightharpoons CaSO_3 + H_2O$

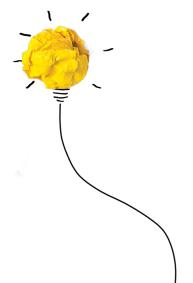
 $CaSO_3 + 1/2 O_2 \rightarrow CaSO_4$

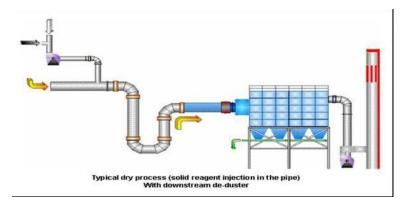
• Treatment by NaHCO₃:

 $NaHCO_3 + HCl \rightleftharpoons NaCl + CO_2 + H_2O$

 $NaHCO_3 + HF \rightleftharpoons NaF + CO_2 + H_2O$

 $2NaHCO_3 + SO_2 + 1/2O_2 \rightarrow Na_2SO_4 + 2CO_2 + H_2O$





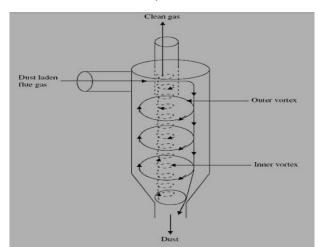
4.Treatment of dust

Particles between 5 & 50 micron and volatized heavy metals



Mechanical treatment : لطرج لميكليكي Cyclone(efficiency:91%)



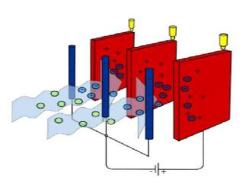


Less than 5 micron



Electrical treatment : علا الإثبار المكلا ج electrostatic precipitator (ESP)(efficiency:95%)







Bottom & flying ashes: heavy metals recovery

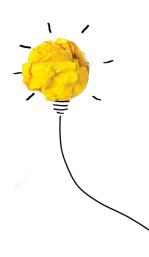
Heavy Metals Recycling Unit for NLAP-IPP Demonstration Plant

(mg/kg)							
Element bottom ash		TOTAL SECTION AND ADDRESS OF	Dry / quasi- dry	wet			
Al	22.000- 73.000	49.000 - 90.000	12.000- 83.000	15777357			
Cd	0.3-70	50- 450	140-300	150- 1.400			
Cu	190-8.200		16- 1.700	440- 2.400			
Fe	4.100- 1500	12.000 - 44.000	2.600- 71.000				
Hg	0,02-8	0,7-30	0,1-51	2,2-2.300			
Мо	2-280	15- 150	9-29	2-44			
Pb	100- 13.700		2.500- 10.000				
Zn	61-7.800	1493597	7.000- 20.000	100000000000000000000000000000000000000			









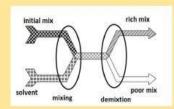
Bottom & flying ashes: heavy metals recovery

Process

Solvent extraction, or liquid-liquid extraction is a separation technique isothermal in a heterogeneous liquid medium.

The method is based on the existence of a difference in the solubility of a substance in two immiscible liquids. The process has three steps, as shown in next figure:

- Mixture of the two immiscible liquids, one of them containing the solute,
- Obtaining physico -chemical equilibrium, leading to demixing , Separation of the two new liquid phases obtained based on the difference of



EXTRACTANTS

Oxime based extractants for copper are largely based on salicyaldoximes which have been modified with one of three modifier types. Examples of the three main extractant types currently in use are:

1. LIX® 984N

A mixture of 2-hydroxy-5-nonylacetophenone oxime and 5-nonylsalicylaldoxime in a high flash diluent. The acetophenone oxime modifies the aldoxime and also performs as an extractant in its own right. Molecular Weight:262.393 g/mol.

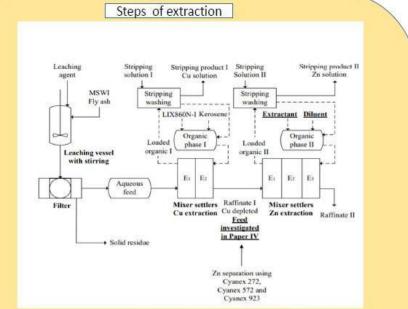
2. Acorga® M5640

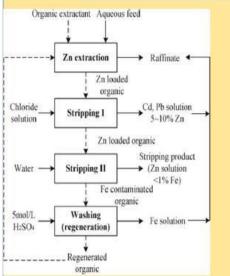
5-Nonylsalicylaldoxime modified with an ester, 2,2,4-Trimethyl-1,3-pentanediol Diisobutyrate (TXIB) in a high flash diluent.

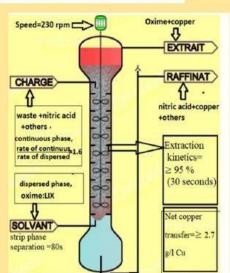
3. LIX® 622N

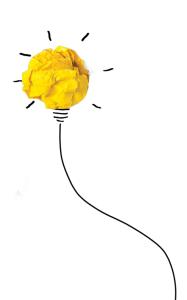
5-Nonylsalicylaldoxime modified with tridecyl alcohol in a high flash diluent.

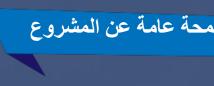
Each of the extractants marketed by the major chemical suppliers has been designed for a specific type of PLS with regard to pH and copper tenor. Used





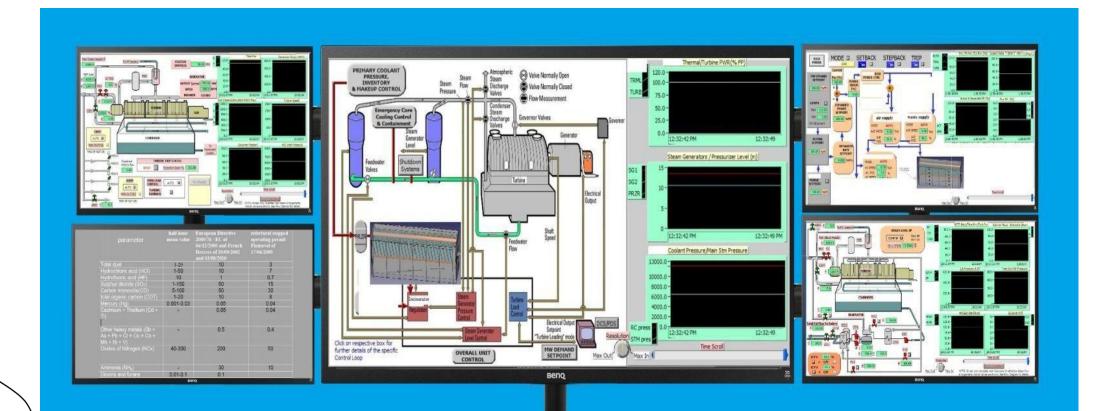




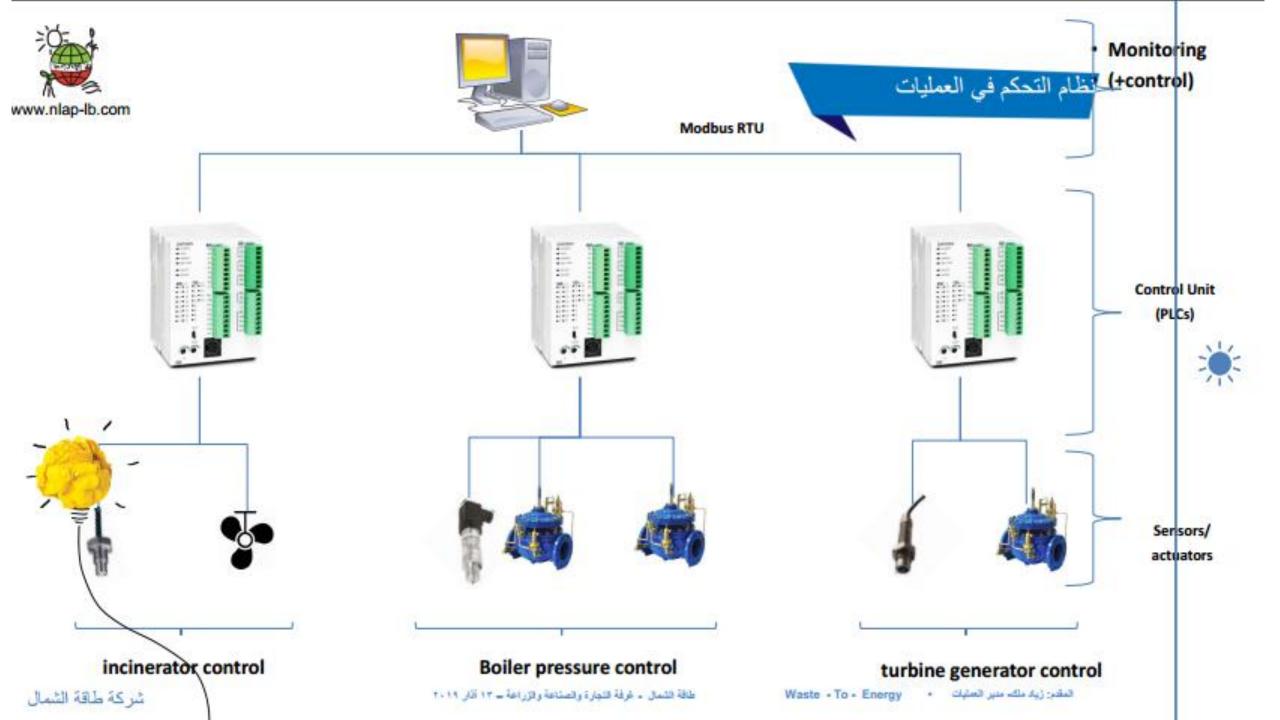




نظام التحكم في العمليات





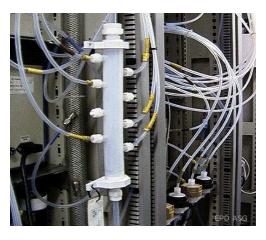






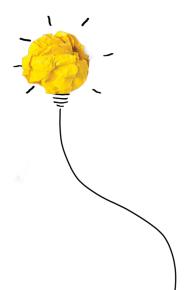
نظام مراقبة تلوث الهواء على امنترنت



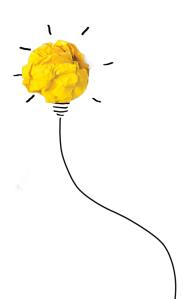








معايير السلامة والبيئة

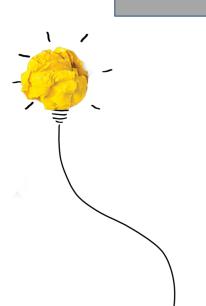


half-hour parameter mean value	European Direc 2000/76 / EC of 04/12/2000 and I Decrees of 20/09 and 03/08/2010	oper French Flam	refectural stopped operating permit Flamoval of 17/06/2009	
Total dust	1-20	10	3	
Hydrochloric acid (HCI)	1-50	10	7	
Hydrofluoric acid (HF)	10	1	0.7	
Sulphur dioxide (SO ₂)	1-150	50	15	
Carbon monoxide(CO)	5-100	50	30	
total organic carbon (COT)	1-20	10	8	
Mercury (Hg)	0.001-0.03	0.05	0.04	
Cadmium + Thallium (Cd + Tl)	-	0.05	0.04	
Other heavy metals (Sb + As + Pb + Cr + Cu + Co + Mn + Ni + V)	-	0.5	0.4	
Oxides of Nitrogen (NOx)	40-300	200	50	
Ammonia (NH ₃)	-	30	10	
Dioxins and furans	0.01-0.1	0.1	-	

معايير السلامة والبيئة

110		<1 ton/n	1-3 (01/11	>3 1011/11
	Elements (polluants)	Maximum value(mg/m ³)	Maximum value(mg/m ³)	Maximum value(mg/m ³)
D	oust	200	100	30
P	b+Cr+Cu+Mn	-	5	5
N	i+As	-	1	1
C	d+Hg	(=	0.2	0.2
C	l (HCl)	250	100	50
F	(HF)	1/ 2	4	2
C	0		300	300

 $\frac{}{}$ - $\frac{}{}$ 300 $\frac{}{}$ 300 Emission limit values in mg m^3 to respected (Lebanese environmental ministry



Pressure equipment shall be designed, manufactured, tested and, if necessary, equipped and installed in such a way as to ensure its safety.

Water tube EN 12952-1 to 17 Shell boiler EN 12953-1 to 14

Design to

the

required

load

capacity:

EN 12952-3

Pressure equipment shall be designed, manufactured, tested and, if necessary, equipped and installed in such a way as to ensure its safety when put into service in accordance with the manufacturer's instructions or under reasonably foreseeable conditions.

Guideline E-03 | Guideline H-07 Guideline H-15 1

تصمم معدات الضغط وتصنع وتختبر ، وإذا لزم الأمر ، مجهزة ومركبة بطريقة تضمن سلامتها عند وضعها في الخدمة وفقاً لتعليمات الشركة الصانعة أه في ظروف معقولة بشكل معقول

In general, a method of calculation according to 2.2.3, supplemented if necessary by an experimental design method

Pressure equipment shall be designed for loads appropriate to its intended use and other reasonably foreseeable operating conditions. In particular, the following factors should be considered:

الضغط الداخلي; nternal and external pressure EN 12952-3 والخارجي: ambient and operating temperatures:

درجات الحرارة المحطة والتشغيلية

Static pressure and filling weights under operating and test conditions:

ضغط ثابت وملء الأوزان تحت ظروف التشغيل والاختيار

Reaction forces and moments related to supporting elements, fixings, piping, etc.; قوات رد الفعل واللحظات المتعلقة بدعم العناصر ، المثبتات

الأنابيب ، وما إلى ذلك corrosion and erosion, material fatigue, etc.:

Decomposition of unstable fluids تحلل السوائل غير المستقرة

In particular, the following applies:

The calculation pressures must not be lower than the maximum allowable pressures, and the static and dynamic fluid pressures as well as the decay pressures of unstable fluids must be taken into account.

The calculation temperatures must have reasonable safety margins.

The maximum stress and stress concentrations must be within safe limits.

-Yield strength, 0.2% or 1% proof strength at the calculation temperature

The operating instructions referred to in section 3.4 must indicate design features that are relevant to the life of the device, for example:

For creep: design life in hours at specified temperatures; For fatigue: design cycle number at specified voltage values; -For corrosion: corrosion surcharge during design.

المتطلبات الكمية الخاصة لمعدات الضغط المحدد650 Special Quantitative Requirements for Specific Pressure Equipment {Guideline H-065

If the elongation at break is greater than 30%:

Or alternatively, if the elongation at break i

Properties Unless other criteria to be considered

require other values, a steel shall be considered to be

sufficiently ductile within the meaning of 4.1 (a) if it

elongation at break is at least 14% in the standard

tensile test and the notch impact work on an ISO-V

sample at a temperature of not exceeding 20 " C. bu

not exceeding 27 J at the intended lowest operating

Re, t (elastic limit) refers to the significant, depending on the material used: following values at the calculation

erritic steel, including normally annealed emperature, depending on the normalized rolled) steel, with the exception of ine grain steel and special heat treated steel: Upper yield strength for /3 of Re, t and 5/12 of Rm, 20; aterials having a lower and Austenitic steel:

3 of Re, t;

pper yield strength; 1.0% proof strength for austenitic nd unalloyed aluminum; 0.2% proof strength in the

bove 35%: 5/6 of Re, t and 1/3 of Rm, t; emaining cases. Unalloyed and low alloy cast steel: 10/19 of Re, Rm. 20 denotes the minimum and 1/3 of Rm 20: value of tensile strength at 20 ° C Rm, t denotes the tensile strength

Aluminum: 2/3 of Re, t; Non-hardenable aluminum alloys: 2/3 of Re, the calculation temperature. nd 5/12 of Rm. 20.

emperature.

Coefficients For welded connections the Not exceed the lower of the following values for onnection coefficients must not exceed the redominantly static loads and at temperatures llowing values outside the range in which creep phenomena are

nspection: 0.7.

or pressure equipment that undergoes destructive and nondestructive tests to verify that the joints are free from significant defects:

For pressure equipment undergoing nondestructive random sampling: 0,85; For pressure equipment which does not undergo non-destructive testing except for visual

necessary, the type of stress and the mechanical and technological properties of the onnection must also be taken into account

miting devices, in particular for pressure vessels The temporary pressure exceeding specified in ection 2.11.2 shall be limited to 10% of the maximum permissible pressure

or pressure vessels, the

ydrostatic test pressure specified section 3.2.2 shall be the nigher of the following:

1.25 times the maximum load of ne pressure equipment in service. aking into account the maximum ermissible pressure and the aximum permissible mperature, or

the 1.43-fold value of the aximum allowable pressure

specified limit.

considered.

a) A compressive strength test designed

to verify that, in the event of pressure

with a margin of safety above the

maximum allowable pressure, the

instrument will not show significant

leakage or deformation beyond a

For the determination of the test pressure,

the differences between the values

measured under test conditions for the

geometrical characteristics and the

material properties on the one hand and

the values permitted for the construction

on the other hand shall be taken into

account: the difference between test and

design temperatures must also be

Fired or otherwise heated overheating-prone pressure equipment in

-a) Appropriate safeguards are provided to limit operating parameters such as heat input, heat output and, where applicable, fluid level to avoid the risk of local or general overheating

(b) where necessary, provide sampling points so that the properties of the fluids can be assessed to avoid risks associated with deposits and / or corrosion;

Reasonable precautions are taken to eliminate the risks of deposit damage: Possibilities for the safe removal of

residual heat after a shutdown are created; -e) measures are taken to prevent the dangerous accumulation of flammable mixtures of flammable substances and air and flashback

The materials used in the manufacture of pressure equipment, unless they are to They must be sufficiently be replaced, must be suitable chemically resistant to for the entire intended service the fluids carried in the life. pressure equipment; the

Welding consumables and other joining materials need only comply with the relevant requirements of sections 4.1, 4.2 (a) and 4.3 first paragraph, both individually and in combination.



The pressure equipment controls shall be such that their operation does not give rise to a reasonably foreseeable hazard. If applicable, the following

chemical and physical

properties required for

operational safety must

not be significantly

impaired during the

c) they must not be

significantly impaired by

intended service life:

points should be noted: -Closing and opening devices;

-Dangerous blow-off from pressure relief valves:

case of overpressure or vacuum in the equipment must be provided:

Surface temperatures taking into account the intended use:

Decomposition of unstable fluids.

a) Pressure equipment shall be designed so that all required safety inspections can be carried out.

o)) Other means to ensure a safe condition of the pressure equipment can be used

necessary, suitable devices for - Devices to prevent physical access in draining and venting the pressure

> To avoid harmful effects such as water hammer, vacuum collapse, corrosion and uncontrolled chemical reactions; all operating and test conditions, in particular pressure tests, must be taken

into accountEN



معايير السلامة والبيئة

تقييم الأثر البيئي لمحطة طاقة كهربائية تعمل على التفكك الحراري للنفايات في سرار - عكار

Environment Impact Assessment (EIA) for an 15 MW waste incineration power plant in Srar/Akkar, Noth Lebanon



من يقوم بالتقييم الأثر البيئي؟ WHO does EIA? صاحب المشروع باستعانة خيراء The project proponent

- To identify and evaluate the predictable environmental consequences of the proposed project the best combination of economic and environmental costs and benefits of the proposed project
 - . وتقييم العواقب البيئية التوقعة للمشروع

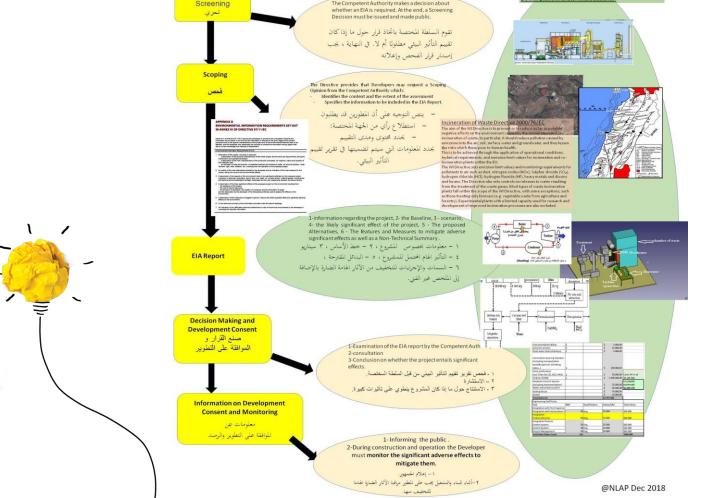
EIA Report for project proposal: 15 MW incineration

أقضل مزيج من التكاليف والقوائد الاقتصادية والبيئية للمشروع المقترح

How is EIA done?

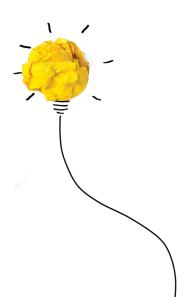
- Identification of the consequences of the project proposal.
- Prediction of the extent of consequences.
- Evaluation of the predicted consequences (Significant or not)
- Mitigation of the adverse consequences.
- Documentation to inform decision makers what needs to be done.

- تحديد نتائج الاقتراح.
 التنبؤ بمدى العواقب.
- تقييم النتائج المتوقعة. (كبير أم لا)
- التخفيف من العواقب السلبية.
- وثائق لإعلام صانعي القرار ما يجب القيام به.



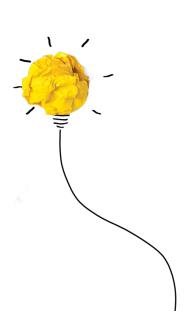
معايير السلامة والبيئة

طرق العمل

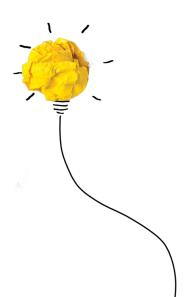


طرق العمل

- 1- شراء محطة
- (OPERATE-BUILT TRANSFER) BOT -2
 - **Managed Services 3**



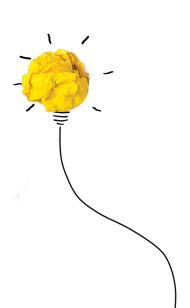
جدوى افتصادية



جدوی اسقتصادیة

شراء المحطة

~3.3 M\$ +10% 5% Annual Maintenance Contract



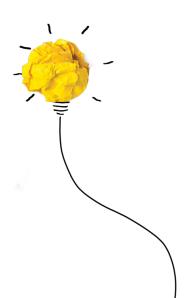
نظام التمويل والمردود المالي المنتظر البلدية لها ٥% من اسهم طاقة الشمال مقابل تقديم الارض للمشروع تصنيع المحظة ٢٠١٧ 1,500,000\$ 1,500,000 \$ شراكة 1,875,000 \$ 2022-2018 1,687,500 \$ (٥ سنوات) 187,500 \$ 2023-2024 1,425,000 \$ 75,000 \$ سنويا انطلاقا من ٢٠٢٥ 750,000 \$

الجدوى الاقتصادية

(Build – Operate – Transfer) BOT

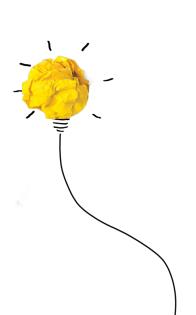
10 years financial plan

القيمة المضافة

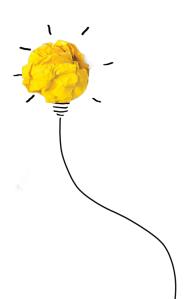


القيمة المضافة

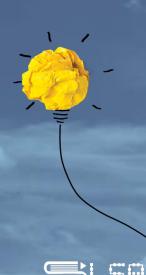
- 1- تامین فرص عمل (5000)
- 2- صناعة محلية لكامل المصنع تكون اوفر
- 3- معالجة لمشكلة النفايات المزمنة في الحال (جبل النفايات النفايات اليومية)
 - 4- تقليل العجز في الكهرباء
 - 5- الاستفادة من بقايا الحرق لصيانة وتعبيد الطرقات
 - 6-اعادة تدوير المعادن
 - -7Local OMC



مناقشة



وشكرا





جدوى القتصادية

1. نظام التحكم في العمليات

